Application No. 10/541,224
Reply to Office Action of May 21, 2008

AMENDMENTS TO THE CLAIMS

1. (Currently amended) A process for production of methanol from a feed stream

rich in hydrogen, carbon monoxide and carbon dioxide, comprising the steps of:

(a) conversion of the feed stream into a converted process stream comprising methanol,

aldehydes and ketones in the presence of a catalyst active in conversion of hydrogen, carbon

monoxide and carbon dioxide into methanol;

(b) first cooling of the converted process stream to obtain a cooled process stream, the

cooled process stream having a temperature of 20-200° C, the temperature being lower than an

exit temperature of the converted process stream during the production of methanol from the

conversion of the feed stream into the converted process stream of step (a);

(c) hydrogenation of the cooled process stream into a hydrogenated process stream rich

in methanol and depleted in aldehydes and ketones in presence of a hydrogenation catalyst active

in conversion of aldehydes and ketones into alcohols, the hydrogenation being carried out in

methanol synthesis gas;

(d) second cooling of the hydrogenated process stream to a cooled, condensed process

stream; and

(e) phase separation of the cooled, condensed process stream into a gas phase and a

liquid crude methanol.

2. (Original) A process according to claim 1, wherein the converted process stream

is cooled to 80-150° C.

3. (Original) A process according to claim 1, wherein the hydrogenation takes

place in a separate reactor.

2

DSMDB-2474215v01

Docket No.: H0610.0385/P385

Application No. 10/541,224 Docket No.: H0610.0385/P385 Reply to Office Action of May 21, 2008

4. (Original) A process according to claim 1, wherein the conversion and the hydrogenation take place in a single reactor.

- 5. (Original) A process according to claim 1, wherein the hydrogenation takes place in a tubular reactor being cooled by a cold feed stream to the conversion.
- 6. (Original) A process according to claim 1, wherein the hydrogenation catalyst is a Cu based catalyst.
- 7. (Currently amended) A process according to claim 6, wherein the Cu content of the hydrogenation catalyst is in the range of 10-95% by weight, preferably 40-70% by weight.
- 8. (Original) A process according to claim 1, wherein the hydrogenation catalyst is a noble metal based catalyst.
- 9. (Original) A process according to claim 1, wherein the hydrogenation catalyst is in the form of pellets, extrudates, monolith, catalysed hardware or a powder suspended in a liquid methanol phase.